

FEED WATER HEATER FOR INCREASING BOILER EFFICIENCY CASE STUDY AT PELW ATTE SUGAR INDUSTRY

A dissertation submitted to the Department of Electrical Engineering, University of Moratuwa in partial fulfilment of the requirements for the Degree of Master of Science

By

JAYAWARDANA MUDIYANSELAGE SAMANKUMARA

Supervised by: Eng. W. D. A. S. Wijayapala.

Department of Electrical Engineering University of Moratuwa Sri Lanka

2010

94551



Abstract

Sugar cane is grown in rural areas in Sri Lanka, and the residue of sugar cane production called bagasse, can be a cheap source of primary boiler fuel, when processing sugar cane. For each 100 tones of sugar cane harvested and milled, 9-10 tones of sugar is produced together with 29-33 tones of solid waste in the form of crushed cane, or bagasse. Typically, the mill uses about 53% of bagasse in a low efficiency steam cycle to produce the electricity and steam which needs for own use. Surplus bagasse is sometimes used for paper making or cattle feed but in Sri Lanka neither of these applications are effectively used. Bagasse is a major bio-mass fuel, which can be used to produce significant quantity of surplus electricity. Progressive sugar cane companies are beginning to see the advantages of creating a substantial additional cash flow by setting up cogeneration power plants fuelled by bagasse.

Using proven technology a 5000 tones/day cane mill can use its own bagasse to supply the mill with steam and power and export approximately 22 MW of electricity. Some large sugar cane mills currently have co-generation power plants that export over 25 MW. In Pelwatte sugar industry, there is 3MW electricity generation and 90T/h steam generation to meet its total demand. Modern conversion systems also ensure lower air emissions meeting latest environmental standards. Because of the harvesting of sugar cane is seasonal, maximum utilization of the co-generation plants is only achieved, if bagasse is stored for use in the off season or other biomass or fossil fuels are employed. Therefore, optimum usage of bagasse is increasing rapidly. If the sugar factory consumes fossil fuels, then those factories are directly affected by the price changes of fossil fuels. For the existence of Sri Lankan sugar industry, and to compete with other sugar industries all over the world, optimum usage of bio-mass usage, such as bagasse is very important.

For the optimum usage of bagasse consumption, various methods can be used. But the sugar factories, which are already installed, have been equipped with some of



University of Moratuwa, Sri Lanka. Electronic Theses & Dissertations www.lib.mrt.ac.lk

these methods. Later modification for optimization and saving of bagasse directly affects the whole system. To optimize bagasse usage, and to minimize fossil fuel usage, it was decided to increase existing boiler efficiency by introducing a feed water heater. But for that, extensive studies were conducted. By this modification it was revealed that an increase of 3% in boiler efficiency could be achieved thereby a saving of 54.2 million LKR could be gained annually. In addition, an obvious reduction of fossil fuel usage and reduction of emissions are the other achievements. Outcomes of this project are significant and it is bound to benefit sugar industry in Sri Lanka.

DECLARATION

The work submitted in this dissertation is the result of my own investigation, except where otherwise stated. It has not already been accepted for any degree, and is also not being concurrently submitted for any other degree.

×

UOM Verified Signature

J. M. Samankumara Date 05/02/2010

l endorse the declaration by the candidate.

UOM Verified Signature Jniversity of Moratuwa, Sri Lanka. Ilectronic Theses & Dissertations Eng. W. D. A. S. Wijayapala Wilb.mrt.ac.lk

Senior Lecturer, Department of Electrical Engineering, University of Moratuwa.

CONTENTS

Page

Declaration			i	
Abstract			iv	
Acknowledgement			v	
List of Figures				
List of Tables				
List of Principal Symbols				
List of abbreviations in				
1.	Introdu	iction	1	
	1.1	Background	1	
	1.2	Motivation	3	
	1.3	Process Description	3	
	1.4	Literature review	3	
	1.5	Goals	4	
2.	Proble	n Statement	6	
3.	Boilers	www.lib.mrt.ac.lk	7	
	3.1	Boiler types	7	
	3.2	Boiler efficiency	8	
	3.3	Methods of increasing boiler efficiency	8	
	3.4	Boiler operating procedures	9	
	3.5	Emissions	10	
	3.6	Control of emissions	11	
4.	Theore	tical Development	14	
	4.1	Data analysis	14	
	4.2	Analysis of selected fuels	16	
	4.3	Overview of existing Boiler	17	
	4.4	Steam flow Diagram	20	
	4.5	Standards	19	
5.	Propos	ed Solution	20	
	5.1	Designing of Feed water heater	20	
	5.2	Proposed feed water heater diagram	21	

5.3 Location of the Feed Water Heater	21	
5.4 Materials	24	
5.5 Diameter of the tubes	24	
5.6 Calculation of heat transfer coefficients	26	
5.7 Calculation of number of tubes required for the feed water heater	28	
5.8 Conditions of feed water after heating	31	
5.9 Dimension of the Heater	32	
5.10 Calculation of side plate's thickness	33	
5.11 Diameter of Bolts	34	
5.12 Deflection of the tubes	35	
5.13 Weight of the heater	35	
5.14 Design of mounting plates	36	
Results and Analysis		
6.1 Water heat recovery & Bagasse saving	37	
6.2 Comparing of Bagasse price with the price of furnace oil	38	
6.3 Calculation of efficiency improvement	38	
6.4 Calculation of material cost & labor cost for a single unit	39	
6.5 Fabrication	40	
6.6 Installation University of Moratuwa, Sri Lanka	41	
Conclusions	42	
7.1 Time Plan	43	
7.2 References	43	
7.3 Appendix	45	

6.

7.

Acknowledgement

Thanks are due first to my supervisor, Eng. W.D.A.S. Wijayapala, Senior Lecturer, Department of Electrical Engineering, University of Moratuwa, **Sri Lanka** for his great insights, perspectives, guidance and sense of humor. My sincere thanks go to the officers in Post Graduate Office, Faculty of Engineering, University of Moratuwa, for helping in various ways to clarify the things related to my academic works in time with excellent cooperation and guidance. Sincere gratitude is also extended to the people who serve in the Department of Electrical Engineering office.

I gratefully thank Dr. Karunadasa, Head of the Electrical Engineering Department, University of Moratuwa for his encouragement, insightful comments, and hard questions.

I gratefully acknowledge Mr. Ariyaseela Wicramanayaka, Managing Director, Mr. Prasad, Group General Manager, and Mr. A. Priyantha, Operational Manager, Pelwatte Sugar Company, Sri Lanka for their advice, supervision, and crucial contribution, which made them a backbone of this project and so to this thesis.

University of Moratuwa, Sri Lanka.

Lastly, I should thank many individuals, friends and colleagues who have not been mentioned here personally in making this educational process a success. May be I could not have made it without your supports.

List of Figures

Figure		Page
3.1	Boiler diagram	7
4.1	Feeding of the Bagasse to the Boiler	16
4.2	Overview of the exiting boiler	17
4.3	Side elevation of the Boiler	18
4.4	Front elevation of the Boiler	18
4.5	Steam flow Diagram	19
5.1	Proposed feed water heater diagram	21
5.2	Location of the Feed Water Heater	22
5.3	The existing arrangement of the feed water to the Boiler Drum	22
5.4	Proposed location of the feed water heater	23
5.5	Air pre-heater tubes	23
5.6	Heater tubes arrangement	26
5.7	Heater tubes	28
5.8	Temperatures at the heater tubes	29
5.9	States of water with temperature onic Theses & Dissertations	31
5.10	Side plates www.lib.mrt.ac.lk	33

List of Tables

Page

4.1	Furnace Oil, Diesel & Bagasse Consumption	14
4.2	Furnace Oil, Diesel Consumption with total sugar cane	15
4.3	Analysis of selected fuels	16
4.4	Ultimate analysis of selected fuels	17
5.1	Energy release and absorption	30
5.2	Steam table	32
6.1	Calculation of material cost	39
6.2	Labor cost for a single unit	40



University of Moratuwa, Sri Lanka. Electronic Theses & Dissertations www.lib.mrt.ac.lk

List of principal Symbols

- u_w _ Velocity of water
- u_f . Velocity of flue gas
- ρ Density kg/m³
- L Length
- V Velocity
- μ Dynamic Viscosity
- Re Reynolds numbers
- N_u Nussel number
- h_f Surface heat transfer coefficient
- D Diameter of the tube
- K Heat transfer conductivity coefficient
- P_r Prandle number
- C₁ Correction factor
- m Mass flow rate
- Cs Specific heat coefficient
- θ temperature difference
- ε Effectiveness of heat transfer Electronic Theses & Dissertations
- C Constant

I - Moment of inertia

- M Bending moment
- σ Stress (nominal)
- w Force per unit area
- d Thickness of the plate
- P Force per unit area
- E Young modulas of elasticity
- δ Deflection

۵

List of Abbreviations

ASTM	- American Society of Testing and Materials Construction
ASME	- American Society for Mechanical Engineers
AWS	- American Welding Society
С	- Carbon
CDM	- Clean Development Mechanism
СО	- Carbon Oxide
CO_2	- Carbon Dioxide
FD	- Forced Draft
Н	- Hydrogen
IRR	- Internal Rate of Return
IPCC	- Intergovernmental Panel on Climate Change
UNFCC	- United Nations Framework Convention on Climate Change
ID	- Induced Draft
Ν	- Nitrogen
NO_2	- Nitrogen Dioxide
PM	- Particulate Matter
S	- Sulfur University of Moratuwa, Sri Lanka.
SO_2	- Sulfur Dioxide
ТОС	- Total Organic Compounds
VOC	- Volatile Organic Compounds