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ANNEXTURE - A

LIST OF SYMBOLS & GLOSSARY

SYMBOLS

1. A = Cross Sectional Area of Extrudate.
2. b = Shape Function.
3. b* = Factor Representing Deformation Occuring in Inlet Zone.
4. Bi = Biot Number.
5. c = Characteristic Relaxation time.
6. C_p = Specific Heat Capacity.
7. D, t = Thickness of Extrudate.
8. G = Elastic Shear Modulus.
9. H₁ = Height of slit die at Land.
10. H₂ = Height of Slit Die, Before Taper Section.
11. H₃ = Equivalent Height of Product.
12. H_E = Height of Slit Die Extrudate at equilibrated Swell State.
13. h_i = Slit or Cone, Die Inlet Height.
14. h_o = Slit or Cone, Die outlet Height.
15. K = Proportionality Factor of Power Law Equation, $\tau = K(\dot{\gamma})^n$
16. K* = Constant related to Short Die Swell Model.
17. L = Length of a Flow Channel.
18. m = Power Law Index of Power Law Equation, $\dot{\gamma} = \phi.(\tau)^m$
19. N = Power Law Index of Power Law Equation, $\tau = K(\dot{\gamma})^n$
20. p = Rheological Parameter Related to Stevenson Die Design Model.
21. q = Rheological Parameter Related to Stevenson Die Design Model.
22. Q = Volumetric Flow Rate. (m³/s)
23. R = Radius of a Flow Channel.
24. r = Rheological Parameter Related to Stevenson Die Design Model.



25. s = Rheological Parameter Related to Stevenson Die Design Model.
26. S, B = Die Swell.
27. $T_{(x,t)}$ = Temperature of The Extrudate at x Distance and at Time t .
28. T_F = Cooling Media Temperature.
29. T_M = Melt Temperature.
30. t_v = Residence Time.
31. V = Volumetric Flow Rate. (mm^3/s)
32. W_1 = Width of Slit Die at Land.
33. W_2 = Width of Slit Die, Before Taper Section.
34. W_3 = Equivalent Width of Product.
35. W_E = Width of Slit Die Extrudate at equilibrated Swell State.
36. z = Distance Along z Axis.
37. ΔP = Pressure Drop.
38. Φ = Degree of Cooling.
39. Θ = Horizontal Convergent Angle of Two Dimensional Converging Flow Channel.
40. α = Size Factor. 
41. α_h = Heat Transfer Coefficient in Calibration Equipment.
42. α_t = Linear Coefficient of Thermal Expansion.
43. α_0 = Half Natural Convergent angle in Extrusion Dies.
44. β = Shape Function.
45. δ = Heat transfer Related Variable.
46. ε = Tensile Strain.
47. $\dot{\varepsilon}$ = Tensile Deformation Rate.
48. ϕ = Proportionality Constant of Power Law Equation, $\gamma = \phi \cdot (\tau)^m$
49. γ = Shear Rate.
50. η = Absolute Viscosity.
51. λ = Thermal Conductivity.
52. μ = Friction Coefficient.

ANNEXTURE - B

LIST OF EQUATIONS

(1). $Q = \frac{\Pi \cdot \Delta P \cdot R^4}{8\eta \cdot L}$

Q = Melt flow rate in a capillary.

Π = A constant.

ΔP = Pressure drop across the capillary.

R = Radius of the capillary.

L = Length of the capillary.

η = Viscosity of the fluid.

(2). $\tau = \eta \cdot \gamma$

τ = Shear stress

η = Viscosity of the fluid.

γ = Shear rate.



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(3). $\sigma = E \cdot \varepsilon$

σ = Tensile Stress

ε = Tensile Rate

E = Tensile Modulus.

(4). $\tau = \eta \cdot \gamma^n$

τ = Shear stress

η = Viscosity of the fluid.

γ = Shear rate.

n = Power Law index

(5). $\Delta P_{\text{Tot}} = \Delta P_{\text{ent}} + \Delta P_{\text{tube}} + \Delta P_{\text{exit}}$

ΔP_{Tot} = Total Pressure Drop

ΔP_{ent} = Entrance Pressure Drop.

ΔP_{tube} = Pressure Drop Due to Flow Resistance.

ΔP_{exit} = Pressure Drop at the Die Exit.

$$(6). \quad Q = [n \cdot \pi R^3 / (3n+1)] \{R \cdot \Delta P / 2KL\}^{1/n}$$

ΔP = Pressure Drop in the Tube.

R = Inside Radius of the Tube.

L = Length of the Tube.

K = Power Law Constant.

n = Power Law Constant.

$$(7). \quad \Delta P/L = [2^{m+1} \cdot (m+2) \cdot V / (\phi \cdot B \cdot H^{m+2})]^{1/m}$$

ΔP = Pressure Drop Across the Rectangular Slit.

L = Length of the Slit.

M = Power Law Index of the Melt.

ϕ = Proportionality Constant in the Power Law.

V = Volumetric Out Put Across the Slit.

B = Breadth of the Rectangular Slit.

H = Height of the Rectangular Slit.

$$(8). \quad \varepsilon_{\text{cone}} = \frac{1}{2} \gamma \tan \omega$$

ε = Extensional strain rate

γ = Shear rate at the exit of the taper

ω = Half angle of taper

$$(9). \quad \varepsilon_{\text{slit}} = \frac{1}{3} \cdot \gamma \tan \omega = \gamma \cdot (h_1 - h_0) / 6L$$

ε = Extensional strain rate

γ = Shear rate at the exit of the taper

ω = Half angle of taper

$$(10). \quad \Delta P_{\text{TOT}} = \Delta P_{\text{ent}} + \Delta P_{\text{land}} + \Delta P_{\text{shear}} + \Delta P_{\text{exit}}$$

ΔP_{TOT} = Total Pressure Drop.

ΔP_{ent} = Entrance Pressure Drop.

ΔP_{land} = Land Pressure drop.

ΔP_{shear} = Pressure Drop due to Shear.

ΔP_{exit} = Pressure Drop At Exit Of The Die

(11). $\Delta P_s = \tau/2n \tan \omega \{1 - (h_0/h_1)^{2n}\}$

ΔP_s = Pressure drop due to shear flow.

τ = Shear Stress

n = Flow behavior index

ω = Half angle of taper

h_0 = Thickness of wedge at Outlet

h_1 = Thickness of wedge at Inlet

(12). $\Delta P_{EXT} = 1/2 \sigma_0 \{1 - (h_0/h_1)^{2n}\}$

ΔP_{EXT} = Pressure drop due to shear flow.

σ_0 = Tensile Stress Corresponding to Tensile Deformation Rate.

n = Flow behavior index

h_0 = Thickness of wedge at Outlet

h_1 = Thickness of wedge at Inlet

(13). $\Delta P = [\eta \cdot \cot \theta (Q(4n+2/W_1 n))^n] [(H_2^{-2n} - H_1^{-2n})/2n * (1+nH_1 \cot \theta / W_1 \cot \Theta) + (H_2^{1-2n} - H_1^{1-2n}) * (n \cot \theta / W_1 (1-2n) \cot \Theta)]$

ΔP = Pressure drop across the wedge.

θ = Vertical taper angle of the wedge.

Θ = Lateral taper angle of the wedge.

n = Power law index.

H_1 = Height of wedge at taller end of the wedge.

H_2 = Height of the wedge at the shorter end of the wedge.

W_1 = Width of the wedge at the shorter end of the wedge.

(14). $n = 1/m$

n, m = Power law indexes used in different equations.

(15). $K = (1/\phi)^{1/m}$

K = Proportionality constant in power law equation.

ϕ = Proportionality constant in power law equation

m = Power law index.

(16). $B_R^2 = 2/3 * \gamma_R [(1+1/\gamma_R)^{2/3} - 1/\gamma_R^3]$

B_R = Swelling Ratio

γ_R = Recoverable Shear Strain.

(17). $G = \tau/\gamma_R$

G = Elastic Shear Modulus

τ = Shear Stress

γ_R = Recoverable Elastic Shear Strain.

(18). $S = a + b^* \cdot e^{(-t_v/c)}$

S = Swelling Potential

a = Velocity Profile

t_v/c = Characteristic Relaxation Time of the Melt

b^* = Representing Factor for Deformation Occurring at the Inlet.

(19). $B = [1 + 3/2 \cdot (n+1) \cdot K \cdot \tan^2 \alpha_0 \cdot (\Delta P_{ENT}/\tau_w)]^{1/2}$

B = Die swell value.

n = Power law index.

$K = L_c/D_c$

α_0 = Half natural convergent angle of polymer melts.

ΔP_{ENT} = Entry pressure drop.

τ_w = Shear stress at the die wall.

L_c = Length of the entry converging region.

D_c = Diameter defined in the diagram.

(20). $\alpha_{ij} = A_i/A_j$

α_{ij} = Size factor between points i and j

A_i = Extrudate cross section at position i.

A_j = Extrudate cross section at position j.

$$(21). \quad \beta_i = X_i/A_i)^{1/2}$$

β_i = Shape factor at point i.

X_i = Characteristic dimension of extrudate at position i.

A_i = Area of extrudate at position i.

$$(22). \quad \beta_{ij} = b_i/b_j = (X_j/X_i)/(A_j/A_i)^{1/2} = X_j/X_i/(\alpha_{ij})^{1/2}$$

β_{ij} = Shape factor between points i and j.

X_j = Characteristic dimension at position i.

X_i = Characteristic dimension at position j.

α_{ij} = Size factor between points i and j.

$$(23). \quad \beta_{ij}^y = [(H_j^y/H_i^y)/(W_j^{xz}/W_i^{xz})]^{1/2}$$

β_{ij}^y = Shape factor between position i and j

H_j^y = Height of channel y at position j

H_i^y = Height of channel y at position i

W_j^{xz} = Width of channel xz at position j

W_i^{xz} = Width of channel xz at position i

$$(24). \quad H_4^y = (\beta_{1E}^y \beta_{E3}^y \beta_{34}^y) (\alpha_{13}^y \alpha_{34}^y)^{1/2} \cdot H_1^y$$

H_4^y = Height of channel y at position 4

β_{1E}^y = Shape factor for channel y between points 1 and E

β_{E3}^y = Shape factor for channel y between points 3 and E

α_{13}^y = Size factor for channel y between points 1 and 3

α_{34}^y = Size factor for channel y between points 3 and 4

H_1^y = Height of channel y at position 1

$$(25). \quad W_E/W_1 = (H_E/H_1)^r$$

W_E = Extrudate width at equilibrated swell state.

w_1 = Width at die.

H_E = Height of product at equilibrated swell state.

H_1 = Height of product at die.

r = Material dependant constant.

$$(26). \quad W_3/W_E = (H_3/H_E)^s$$

W_E = Extrudate width at equilibrated swell state.

W_3 = Product width.

H_E = Height of extrudate at equilibrated swell state.

H_1 = Height of die.

s = Material dependant constant.

$$(27). \quad Q^y = W_1^y \cdot (H_1^y)^2 / F(n) \{ H_1^y \cdot \Delta P / (2m^* \cdot L_1^y) \}^{1/n}$$

Q^y = Volumetric out Put Across the Channel y.

W_1^y = Width of the Channel.

H_1^y = Height of the Channel.

$F(n) = 2 \cdot (1/n+2)$

ΔP = Pressure Drop Across the Channel.

m^* = Rheological Parameters of the Melt.

L = Length of the Channel.

n = Power Law Index.

$$(28). \quad H_E/H_1 = [1 + p \cdot (\tau)^q]^{1/4}$$

p = Width of Slit at Product.

$\tau = \Delta P H_1 / 2L_1$, Shear Stress Applied in the Slit.

H_E = Height of Slit at Equilibrated Swell State

H_1 = Height of Slit at Die

q = Constant.

$$(29). \quad \tau = \Delta P \cdot H / 2 \cdot L$$

τ = Shear Stress

ΔP = Pressure Drop Applied Across the Flow channel.

H = Height of the Channel.

L = Length of the Channel.

$$(30). \beta_{1E}^y = [(H_E^y/H_1^y)/(W_E^{xz}/W_1^{xz})]^{1/2} = [1+p(\tau^y)]^{(1-r)/8}$$

β_{1E}^y = Shape Factor for Channel y, Between Points 1 & E.

p = Constant Depending on Rheological & Die Swell Properties.

τ^y = Shear Stress Applied in Section Y.

r = Constant

$$(31). \beta_{E3}^{xz} = [(H_E^{xz}/H_1^{xz})/(W_E^y/W_1^y)]^{1/2} = [\beta_{1E}^y]^{-1}$$

β_{E3}^y = Shape Factor For Channel Y, Between Points E & 3.

α_{E3}^y = Size Factor For Channel Y, Between Points E & 3.

s = Constant Depending on Rheological & Die Swell Properties.

$$(32). \alpha_{1E}^y = (1+p \cdot (\tau)^q)^{(r+1)/4}$$

α_{1E}^y = Size Factor for Channel y.

p = Constant Depending on Rheological & Die Swell Properties.

q = Constant Depending on Rheological & Die Swell Properties.

r = Constant Depending on Rheological & Die Swell Properties.

$$(33). \alpha_{13}^y = \{H_1^y/(U_3 \cdot F(n))\} \cdot \{\tau_y/m^*\}^{1/n}$$

α_{13}^y = Size Factor for Channel y, between points 1 & 3.

H_1^y = Height of the Channel.

U_3 = Die Exit Velocity.

$F(n) = 2 \cdot (1/n + 2)$

τ_y = Shear Stress Applied in Channel Y.

m^* = Constant.

n = Power Law Index.

$$(34). \beta_{E3}^y = [\alpha_{E3}^y]^{(1-s)/2(s+1)}$$

β_{E3}^y = Shape Factor For Channel Y, Between Points E & 3.

α_{E3}^y = Size Factor For Channel Y, Between Points E & 3.

s = Constant Depending on Rheological & Die Swell Properties.

(35). $\alpha_{E3}^Y = \alpha_{13}^Y / \alpha_{1E}^Y$

α_{E3}^Y = Size Factor for Channel y, between points E & 3.

α_{13}^Y = Size Factor for Channel y, between points 1 & 3.

α_{1E}^Y = Size Factor for Channel y, between points 1 & E.

(36). $H_3^Y / H_1^Y = \beta_{1E}^Y \beta_{E3}^Y (\alpha_{13}^Y)^{1/2}$

H_3^Y = Product Thickness at Position Y.

H_1^Y = Die Thickness at Position Y.

β_{1E}^Y = Shape Factor Between Die and Equilibrated State at Position Y.

β_{E3}^Y = Shape Factor Between Equilibrated State and Product at Position Y.

α_{13}^Y = Size Factor Between Die and Product at Position Y.

(37). $W_3^{XZ} / W_1^{XZ} = \beta_{1E}^{XZ} \beta_{E3}^{XZ} (\alpha_{13}^Y)^{1/2}$

W_3^{XZ} = Product Width at Position XZ.

W_1^{XZ} = Die Width at Position XZ.

β_{1E}^{XZ} = Shape Factor Between Die and Equilibrated State at Position XZ.

β_{E3}^{XZ} = Shape Factor Between Equilibrated State and Product at Position XZ.

α_{13}^Y = Size Factor Between Die and Product at Position Y.

(38). $\tau_{wall} = -p \cdot \mu_G \cdot \exp[(2\mu_G/R) \cdot (L-z)]$

R = Radius of the tube.

P_L = Melt pressure at distance L.

μ_G = Friction coefficient in slipping.

μ_H = Friction coefficient in adhesion.

τ_{crit} = Critical wall stress.

(39). $\Phi = (T_{(x,t)} - T_F) / (T_M - T_F)$

T_M = Melt temperature.

T_F = Cooling media temperature.

$T_{(x,t)}$ = Temperature of the extrudate at x distance and at time t.

$$(40). \quad (T_{(x,t)} - T_F) / (T_M - T_F) = [2\text{Sin}\delta / (\delta + \text{Sin}\delta \cdot \text{Cos}\delta)] \cdot e^{-\delta^2 a t / D^2} \cdot \text{Cos}(\delta \cdot x / D)$$

$T_{(x,t)}$ = Temperature at melt / frozen melt interface.

T_F = Temperature of Cooling Fluid.

T_m = Temperature of Melt.

δ = Dimensionless Parameter.

a = $\lambda / \rho \cdot C_p$

t = Time Taken to Form a Required Thickness of Frozen Melt.

D = Wall Thickness of the Extrudate.

x = Thickness of Frozen Melt.

$$(41). \quad \alpha_h \cdot D / \lambda = \text{Bi}$$

α_h = Heat transfer coefficient

D = Wall thickness of the extrudate.

λ = Thermal conductivity

Bi = Biot number

$$(42). \quad \delta = \alpha_h D / \lambda \cdot \cot \delta.$$

δ = Dimensionless Parameter.

α_h = Heat Transfer Coefficient

D = wall Thickness of the extrudate

λ = Thermal Conductivity

$$(43). \quad v(T) = 1 / \rho(T)$$

$v(T)$ = Volume of melt at temperature T.

$\rho(T)$ = Density of melt at temperature T.

$$(44). \quad \rho(T) = \rho(T_0) * 1 / (1 + \alpha_t(T - T_0))$$

α_t = Linear coefficient of thermal expansion

$\rho(T_0)$ = Density at the reference temperature T_0

$\rho(T)$ = Density at temperature T

(45). $L_2 = l_1(1 + \alpha_1 \Delta T)$

ΔT = Temperature difference

α_1 = Thermal expansion coefficient

L_2 = Length of extrudate at melt temperature.

l_1 = Length of solidified extrudate at room temperature.

(46). $\tau = \Delta P.H/2.L$

ΔP = Pressure Drop Across the Slit.

τ = Shear Stress Applied.

L = Length of Slit Channel.

H = Height of Slit Channel.

(47). $V_z = (\phi/m+2).(\Delta P/L)^m.(H/2)^{m+1}$

V_z = Average Velocity at the Slit.

ϕ = Proportionality Constant of Power Law Equation.

m = Power Law Index.

ΔP = Pressure Drop Across the Slit.

L = Length of Slit.

ANNEXTURE - C

LIST OF FIGURES

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ANNEXTURE – D

DERIVATION OF PRESSURE DROP EQUATION FOR TAPERED CHANNELS; REF: EQUATION (13).

Pressure Drop for a Parallel Slit Channel;

$$\Delta P = 2 \eta L (\xi + 1) \{Q(4n+2)/n\}^n \cdot \xi^{-(n+1)} \cdot H^{-(3n+1)} \quad (13.1)$$

$\xi = W/H$, Shape Factor.
 η = Viscosity of the Melt.
 L = length of Slit.
 Q = Volumetric Out Put.
 n = Power Law Index.
 H = Height of Slit.

Tapering rectangular Channel,

Consider a tapering channel of constant cross sectional rectangular shape. The height h , at any point along the length l , is defined by,

$$h = H_1 - 2.l.\tan\theta \quad (13.2)$$

$$\xi h = \xi H_1 - 2.l.\tan\phi \quad (13.3)$$

Where, θ and ϕ are the vertical and lateral taper angles.

Similarly, $\xi = \cot\theta/\cot\phi$,
 From (A2), $dl = -(dh/2) \cdot \cot\theta$ (13.4)

Incremental Pressure drop dP is obtained by, substituting dl for L and h for H , and integration between limits H_1 & H_2 yields,

$$\Delta P = (\eta \cdot \cot\theta/3) (\xi + 1) \xi^{-(n+1)} \{Q \cdot (4n+2)/n\}^n [H_2^{-3n} - H_1^{-3n}] \quad (13.5)$$

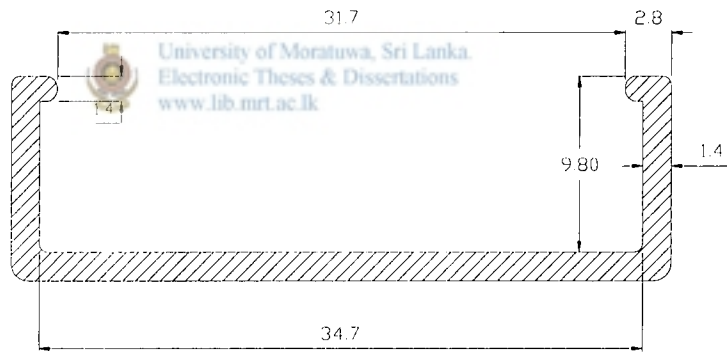
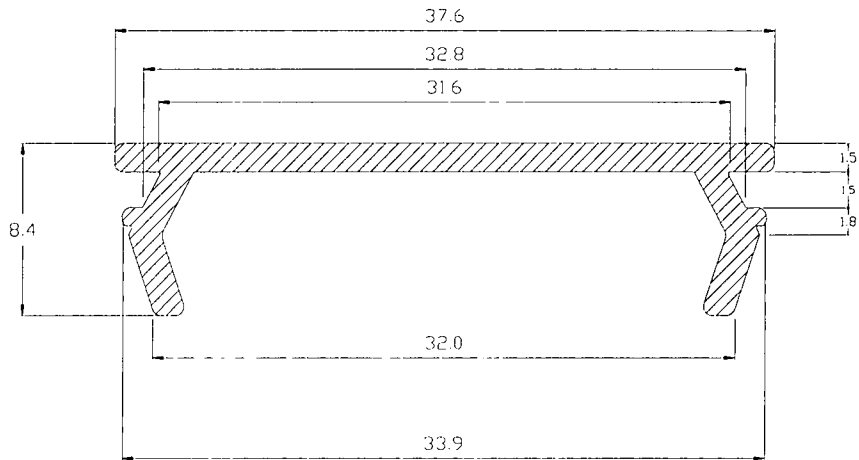
Taking ξ , as a constant, simplifying using binomial theorem gives, (A6);

$$\Delta P = [\eta \cdot \cot\theta (Q(4n+2)/W_1 n)^n] [(H_2^{-2n} - H_1^{-2n})/2n + (1+nH_1 \cot\theta/W_1 \cot\phi) + (H_2^{1-2n} - H_1^{1-2n}) \cdot (n \cot\theta/W_1 (1-2n) \cot\phi)] \quad (13)$$

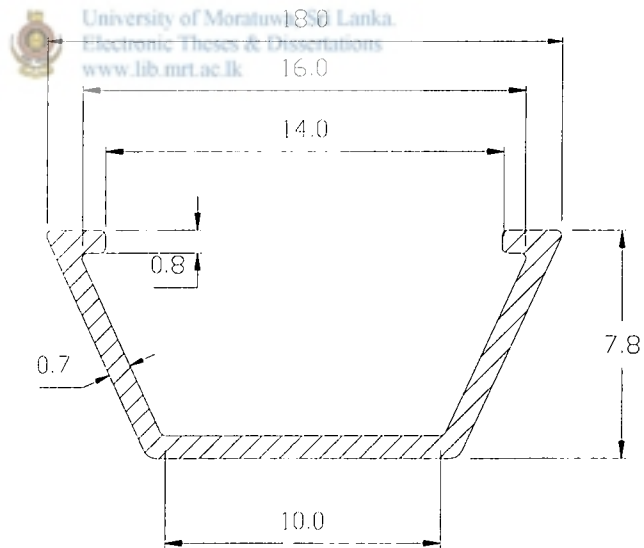
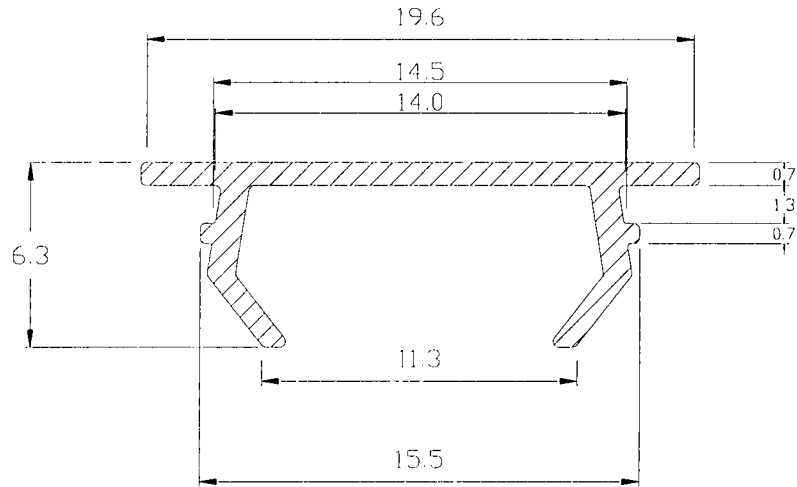


ANNEXTURE - E

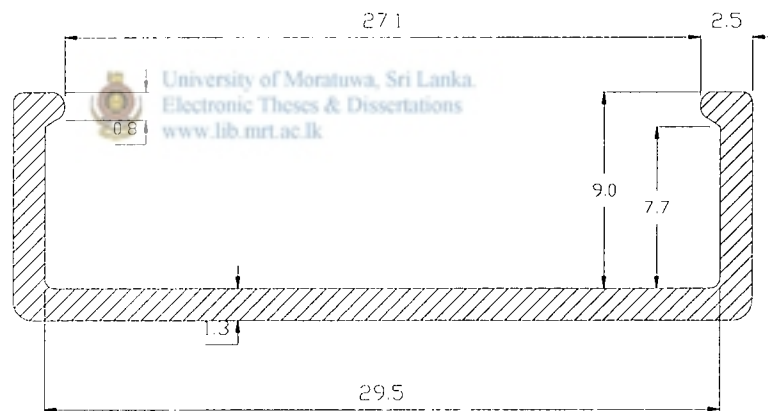
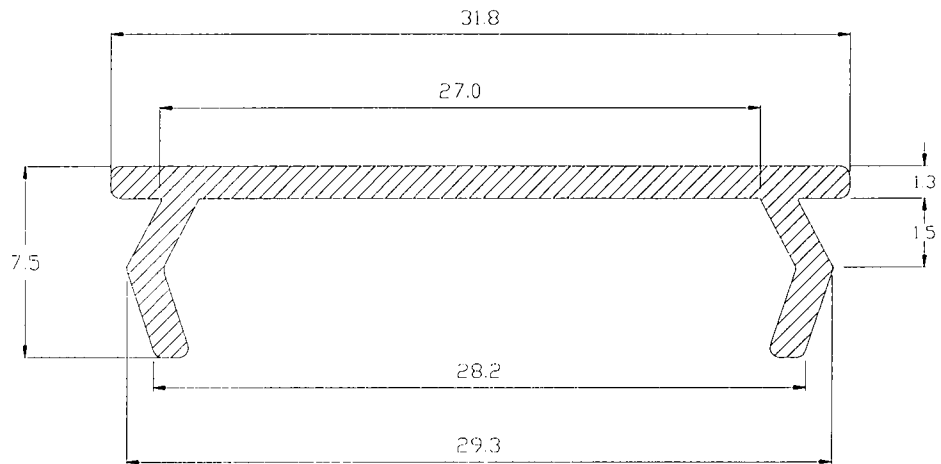
CROSS SECTION OF A TRUNKING PROFILE IN THE MARKET (BRAND A)



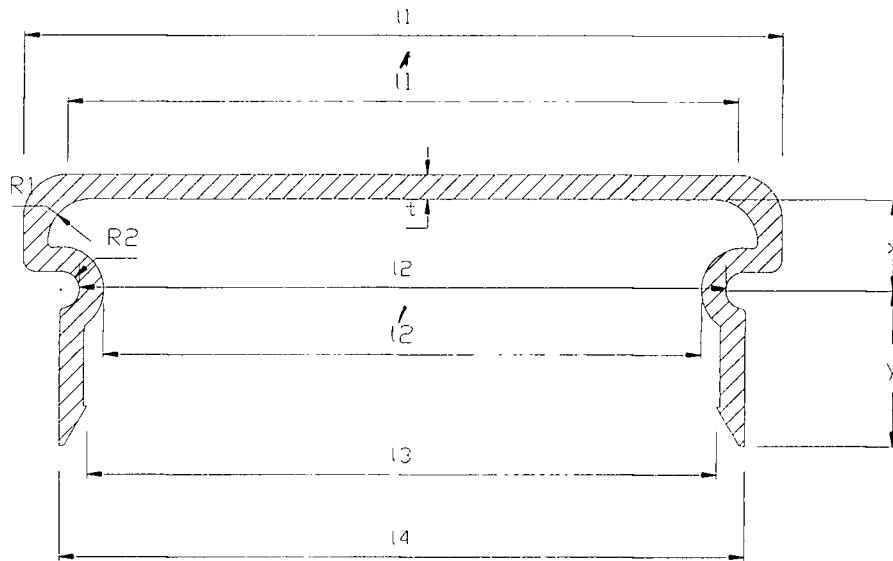
ANNEXTURE - F
CROSS SECTION OF A TRUNKING PROFILE IN THE MARKET (BRAND B)



ANNEXTURE - G
CROSS SECTION OF A TRUNKING PROFILE IN THE MARKET (BRAND C)



ANNEXTURE – H
DESIGNED PRODUCT DIMENSIONS & DRAWINGS




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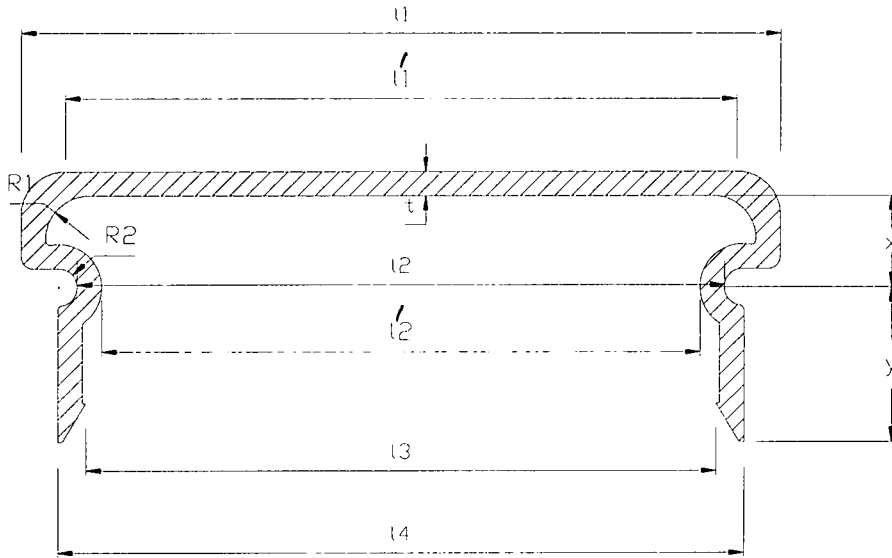
All dimensions are in mm

l_1	l_2	l_1'	l_2'	l_3	l_4
31.3	26.9	28.2	26.1	1.5	1.05

t	R_1	R_2	X	Y	
1.05	2.0	2.0	3.0	6.0	



ANNEXTURE – I
DESIGNED PRODUCT, DIE, CALBRATOR DIMENSIONS



R1 – Outer Surface Radius
 R2 – Inner Surface Radius

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Units in mm

	Die	Equilibrated Swell State	Product
l_1	31.28	31.33	31.30
l_1'	29.22	29.17	29.20
l_2	26.88	26.93	26.90
l_2'	24.82	24.77	24.80
l_3	28.22	28.17	28.20
l_4	26.08	26.13	26.10
x	3.03	2.98	3.00
y	6.00	6.02	6.00
R1	2.00	1.98	2.00
R2	2.00	2.02	2.00
t	1.03	1.08	1.05



ANNEXTURE - S

APPROXIMATION OF PROFILE DIE DIMENSIONS TO A SLIT DIE.

1.0 Product Die Dimensions;

$$\begin{aligned} & \text{Width of Equivalent slit die, (Ref. Annex. - H)} \\ & = 2x\{6.00 - 2.00 + 3.14x2.00 + 1/4x2x3.14x2.00\} + 29.2 - 2x2.0 \\ & = 2x\{4.00 + 3.14(2+1)\} + 25.20 \\ & = \mathbf{52.04 \text{ mm}} \end{aligned}$$

$$\begin{aligned} & \text{Height of Equivalent slit die, (Ref. Annex - H)} \\ & = \text{Thickness of the product.} \\ & = \mathbf{1.05 \text{ mm}} \end{aligned}$$

2.0 Die Land Dimensions;

$$\text{Width of Equivalent Slit Die} = \mathbf{52.14 \text{ mm}}, \text{ (Ref. 6.3)}$$

$$\text{Height of Equivalent Slit Die} = \mathbf{1.03 \text{ mm}}, \text{ (Ref. 6.3)}$$

3.0 Die Dimensions, Parallel Section Before the Taper;

$$\begin{aligned} \text{Width of Equivalent Slit Die} & = 52.04 + 7.05 \text{ mm (Ref. 8.0 \& 6.0)} \\ \text{(Taper Angle } 10^\circ) & \qquad \qquad \qquad = \mathbf{59.09 \text{ mm}} \end{aligned}$$

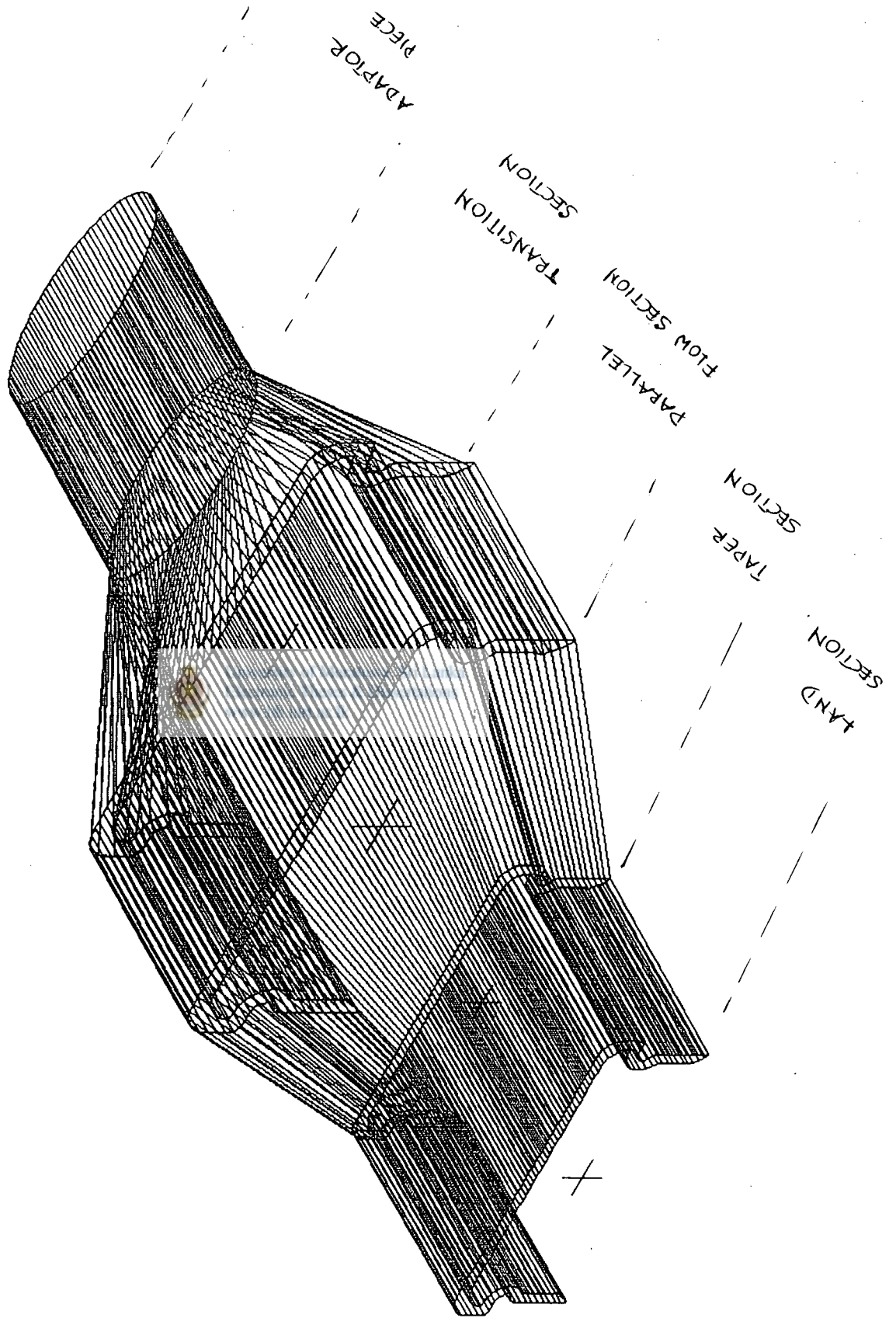
$$\begin{aligned} \text{Height of Equivalent Slit Die} & = 1.05 + 7.05 \text{ mm (Ref. 8.0 \& 6.0)} \\ \text{(Taper Angle } 10^\circ) & \qquad \qquad \qquad = \mathbf{8.10 \text{ mm}} \end{aligned}$$

4.0 Equilibrated Swell State Slit Profile Dimensions;

$$\text{Width of the Equilibrated Slit Die} = \mathbf{53.03 \text{ mm}} \text{ (Ref. 6.3)}$$

$$\text{Height of the Equilibrated Slit Die} = \mathbf{1.07 \text{ mm}} \text{ (Ref. 6.3)}$$

DIE LAYOUT OF THE DESIGNED PROFILE EXTRUSION DIE



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